

In Situ Chemical Oxidation Through Lance Permeation at the Portsmouth Gaseous Diffusion Plant (PORTS)

M. Z. Martin
O. R. West

Environmental Sciences Division



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Environmental Sciences Division

**IN SITU CHEMICAL OXIDATION THROUGH LANCE
PERMEATION AT THE PORTSMOUTH GASEOUS
DIFFUSION PLANT (PORTS)**

M. Z. Martin

O. R. West

Environmental Sciences Division
Oak Ridge National Laboratory

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ABSTRACT

In situ chemical oxidation through lance permeation (ISCO-LP) is an emerging remediation technology in which chemical oxidants (such as potassium or sodium permanganate) are delivered to the subsurface using vertical lance-like injectors. It is applicable to sites with oxidizable contaminants such as chlorinated solvents and fuel hydrocarbons. Because vertical lance injections can be deployed at relatively close spacing, ISCO-LP potentially can be used to clean-up contamination in low-permeability media.

This document provides information that can help potential users determine whether ISCO-LP would apply to a particular environmental management problem. It contains a general description of the technology (Section 2), performance data from a field demonstration (Section 3), an assessment of technology applicability (Section 4), a summary of cost elements (Section 5), and a list of regulatory, environmental safety and health issues (Section 6). It is patterned after the Innovative Technology Summary Reports (ITSR) published by the Department of Energy's (DOE) Office of Science and Technology under the Subsurface Contaminants Focus Area (SCFA). As in the previously published ITSRs, the technology described in this report was developed through funding from SCFA.

Most of the information contained in this report was obtained from a field demonstration of ISCO-LP conducted in July-August 2000 at DOE's Portsmouth Gaseous Diffusion Plant (PORTS). The field test was not completed due to an accident that caused a field worker serious injuries. Although performance assessment data are very limited, the field test highlighted important health and safety issues that must be considered by site managers and technology vendors interested in implementing ISCO-LP.

1. TECHNOLOGY DESCRIPTION

In situ chemical oxidation (ISCO) is a rapidly developing class of remediation technologies in which oxidants (e.g., potassium or sodium permanganate, KMnO_4 or NaMnO_4) and hydrogen peroxide (H_2O_2) are delivered to the subsurface to degrade organic contaminants such as trichloroethylene (TCE) and tetrachloroethylene (PCE) (Schnarr et al., 1998; Siegrist et al., 2001). The oxidation of TCE by MnO_4^- follows a series of sequential reactions, beginning with the rate-limiting formation of a cyclic hypomanganese ester, followed by the rapid decomposition of the ester into carboxylic acids that are then more slowly oxidized by MnO_4^- to the final product, CO_2 . From a practical perspective, TCE degradation has been shown to occur relatively rapidly in batch tests where >99% reduction in TCE concentration was achieved within 24 hours in soils treated with concentrated MnO_4^- solutions (Gates et al., 2000). These tests also show that MnO_4^- generally resulted in more extensive degradation of TCE and PCE under a wider range of subsurface conditions when compared to H_2O_2 .

KMnO_4 and NaMnO_4 are inherently more stable than H_2O_2 , the latter tending to decompose rapidly to H_2O and O_2 when brought in contact with soil material. NaMnO_4 is significantly more soluble than KMnO_4 (~65% vs ~7% at room temperature), which allows it to be delivered in more concentrated solutions. This is particularly important in situations where high pore water saturation limits the volume of oxidant that can be injected into the subsurface. Because highly concentrated NaMnO_4 solutions can be used, more care is needed in handling such a reactive fluid in the field. There is also no radioactivity associated with NaMnO_4 , whereas there is a small fraction [0.0117%] of K-40 in KMnO_4 . This slight radioactivity posed logistical difficulties at the Portsmouth Gaseous Diffusion Plant, where field methods

used to screen for radioactivity could not distinguish between K-40 and other radionuclides. Because waste disposal criteria at the plant were based on these field methods, piping used to deliver KMnO_4 solutions had to be disposed of as radioactive waste.

As in most in situ remediation technologies involving chemical reagents, effective delivery of the chemical oxidant solution to the subsurface is the key to a successful implementation of ISCO. In previous ISCO field demonstrations, permanganate oxidants were injected into the subsurface using horizontal and vertical wells (West et al. 1997, Lowe et al. 2002). Such an approach would not be effective in fine-grained sediments where oxidant transport is severely limited by low hydraulic conductivities. Lance permeation involves the use of closely spaced vertical lances to penetrate the subsurface to depths of up to 40 ft. From each lance tip, oxidant can be injected under pressure into the soil at specified depth intervals providing oxidant delivery and distribution. Spacing of the lances and injection depth intervals can be adjusted depending on site conditions, and can be as small as 2 to 3-ft in low-permeability clays. Using lance permeation, targeted delivery of oxidants to source zones or hot spots is feasible even in tight clays.

When designing a lance permeation treatment scheme, primary consideration is given to injection spacing (horizontal and vertical), pressures, and volumes of oxidant solutions. The latter is determined by the amount required to treat expected contaminant levels through out a target area, as well as provide excess oxidant to be consumed by natural organic matter. It is not always necessary for the entire subsurface to be saturated with oxidant. Concentrated oxidant solutions can be delivered into discrete intervals and allowed to diffuse into the surrounding matrix. Injection spacing can be decreased in areas of higher contaminant concentrations and/or low soil moisture content while increased in areas of lower contaminant concentrations and/or high soil moisture content. The depth of injection limits injection pressures to avoid excessive leakage of the oxidant to the surface.

2. PERFORMANCE: AUGUST 2000 FIELD TEST AT PORTS

2.1 BACKGROUND

A field demonstration of ISCO-LP was conducted in the summer of 2000 at DOE's PORTS-site, which is located approximately 80 miles south of Columbus, 20 miles north of Portsmouth, and 1 mile east of U. S. Route 23, near Piketon in south-central Ohio (Fig. 1). Personnel from Oak Ridge National Laboratory (ORNL) provided technical oversight for the field demonstration as well as pretreatment soil and groundwater characterization. International Technology Corporation (ITC, Knoxville, TN) was the vendor selected for actual execution of ISCO-LP, based a competitive bidding process. ITC designed the specific details of the field test, based on general specifications provided by ORNL. Lance permeation was conducted using a Geoprobe drill rig owned and operated by Miller Drilling Co., Inc. As described in Section 3.5, the field test was aborted due to an accident that seriously injured a field worker. Approximately 1 year after the aborted field test, Environmental Quality Midwest, Inc. (EQM)/CDM Federal designed and executed post-treatment soil and groundwater sampling to evaluate the effects of ISCO-LP on TCE contamination and residual Mn within the zone actually treated.

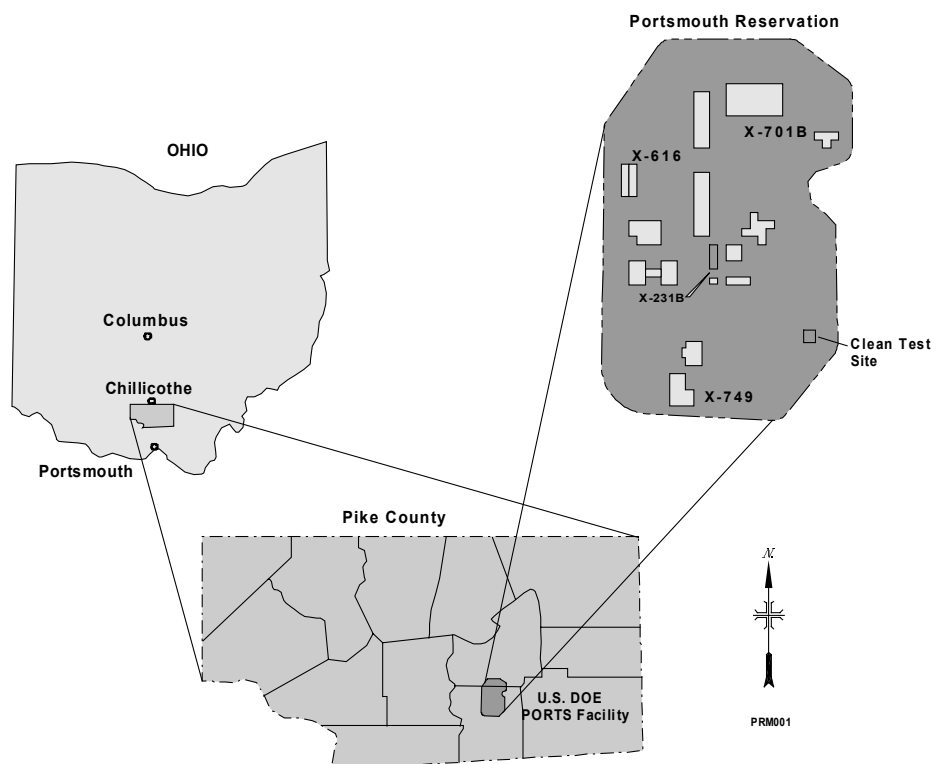
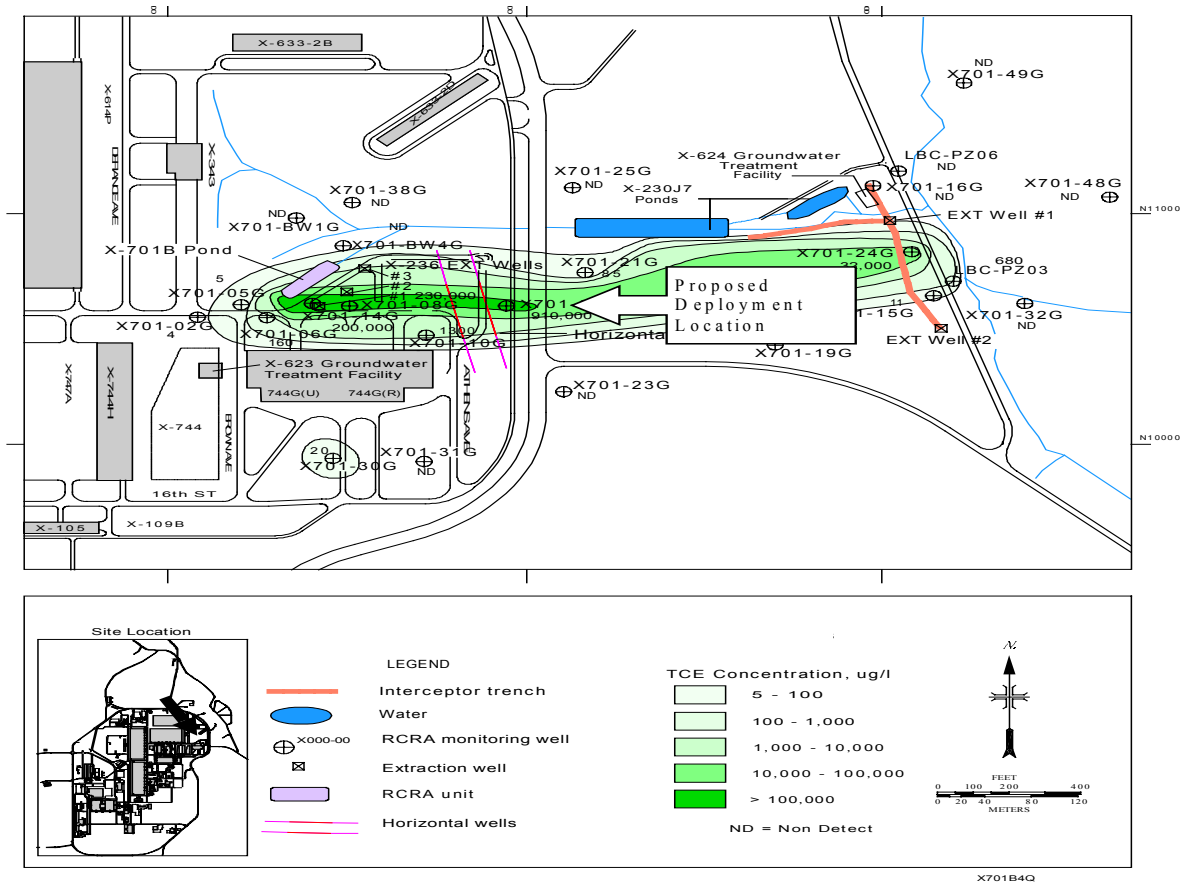
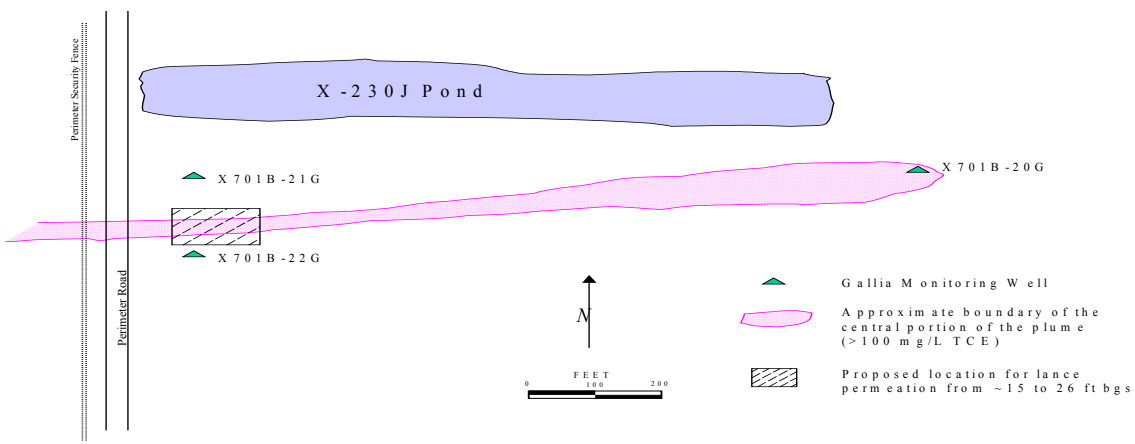


Fig. 1. Location of the Portsmouth Gaseous Diffusion Plant

The X-701B plume area (Fig. 2) within PORTS was chosen as the specific field test site to take advantage of knowledge gained from previous demonstrations at this location (West et al. 1997, Korte et al. 1997). Initial contamination at the site is believed to be from an unlined holding pond that was used for neutralization and settling of metal-bearing acidic wastewater and solvent contaminated solutions. The holding pond was drained and the contaminated sludge and underlying silt and clay were removed as part of a RCRA closure action in 1990. However, recent sampling in the area shows residual TCE contamination in the sediments, as well as a groundwater plume in the underlying silty-gravel aquifer that still persists (Fig. 2), and is migrating offsite in an east-west direction following the general groundwater flow.



(a)



(b)

Fig. 2. The X-701B Plume at PORTS (a) and ISCO-LP field test deployment location (b).

2.2 SITE HYDROGEOLOGY

The stratigraphy underlying the X701-B site consists of the following layers in descending order: (1) the Minford Unit with a thickness of 25 to 30 ft, (2) the Gallia Unit with a thickness varying from 2 to 10 ft, (3) the Sunbury shale formation (10 to 15-ft thick), and (4) Berea sandstone which is present at an approximate depth of 47 ft in this area. The Minford Unit is divided into an upper clay and a lower silty zone. The Minford upper zone ranges in thickness from 12 to 20 ft and generally consists of stiff, silty clay. The Minford lower silt layer is 8.5 to 18 ft thick.

The Gallia Unit, which lies beneath the Minford, is composed of reddish-brown silty, clayey sand and gravel. The Gallia, which is the primary pathway for groundwater contaminant migration, has a relatively high hydraulic conductivity that varies greatly from <1 ft/d to over 400 ft/d. The hydraulic conductivity of the Minford silt member ($\sim 10^{-3}$ ft/d) is significantly lower than that of the underlying Gallia unit, but is higher than that of the overlying Minford clay member ($\sim 10^{-4}$ ft/d). The Gallia unit and the saturated portion of the Minford silt member act as a single water-bearing unit confined above and below respectively by the Minford clay member and the Sunbury Shale formation. Based on groundwater sampling, the latter shale formation has effectively prevented downward migration of contaminated groundwater from the Gallia into the underlying Berea sandstone. The target units for the ISCO-LP field test were the saturated Minford and Gallia. Depth to water within the test site is ~ 12 ft. Depth to the Gallia and Sunbury Shale (i.e., bedrock) are ~ 25 and ~ 32 ft, respectively. Pretreatment sampling at the field site showed TCE contamination in the saturated Minford and Gallia sediments ranged from 34 to 369,000 $\mu\text{g}/\text{kg}$ with concentrations consistently increasing with depth. More details regarding pretreatment contaminant concentrations are provided in Section 3.4

23 FIELD TEST OPERATIONS

The initial plan for the field test was to deliver a 2% NaMnO_4 solution using lance permeation to the Minford and Gallia over a 180 ft x 80 ft area (Fig. 2b). The area was divided into a 10-ft x 10-ft grid and injection points were to be located at the grid nodes. Oxidant was to be injected at 18 to 24-in depth intervals beginning at the water table (~ 15 ft bgs) through the saturated Minford and Gallia to the top of the Sunbury to determine the applicability of lance permeation at greater depths and in coarser subsurface soils (i.e., gravels).

Only 44 of the 144 planned injections were completed before the field test was aborted. Because of the accident and aborted work, process details regarding the completed injections (such as oxidant volumes and injection pressures) are not available.

2.4 PRE- AND POST-TREATMENT MONITORING RESULTS

Pre-treatment sample collection from 20 boreholes and sample analyses were completed before the field test was aborted. The pretreatment samples were collected by ORNL using the Geoprobe/Terraprobe sampling method at ~ 2 ft depth intervals from ~ 15 ft to 32 ft bgs. Each sample was analyzed on-site for TCE and other selected chlorinated hydrocarbons using hexane extraction and a gas chromatograph equipped with an electron capture detector. Onsite sample analysis and sample handling techniques were used to minimize negatively biased TCE analysis results due to volatilization losses. Sediment samples from a number of borings were analyzed for Mn and other metals.

A year after the aborted field test, EQM/CDM was contracted by Bechtel Jacobs to design and execute post-treatment sampling at the ISCO-LP field test site. Borings for the post-treatment samples were generally collocated with the pre-treatment boreholes, but sampling depth intervals were fixed at 9, 28, and 33 ft. Post-treatment sediment samples were collected using a split spoon sample, and samples were analyzed for VOCs and metals at an offsite laboratory. Exact procedures used for handling and preparation of post-treatment samples are not available.

Comparison of the limited post-treatment with pre-treatment performance data shows generally lower TCE concentrations after ISCO-LP (Appendix A). The treatment appeared to be quite effective in degrading TCE within the Gallia, based on a comparison of paired samples at 28 ft (i.e., below the water table) collected before and after treatment (Fig. 3). Unfortunately, the post-treatment samples from the Minford were all collected at 9 ft, well above the shallowest oxidant injection depth (at 15 ft bgs). Thus, the effectiveness of ISCO-LP in the low-permeability Minford could not be objectively assessed.

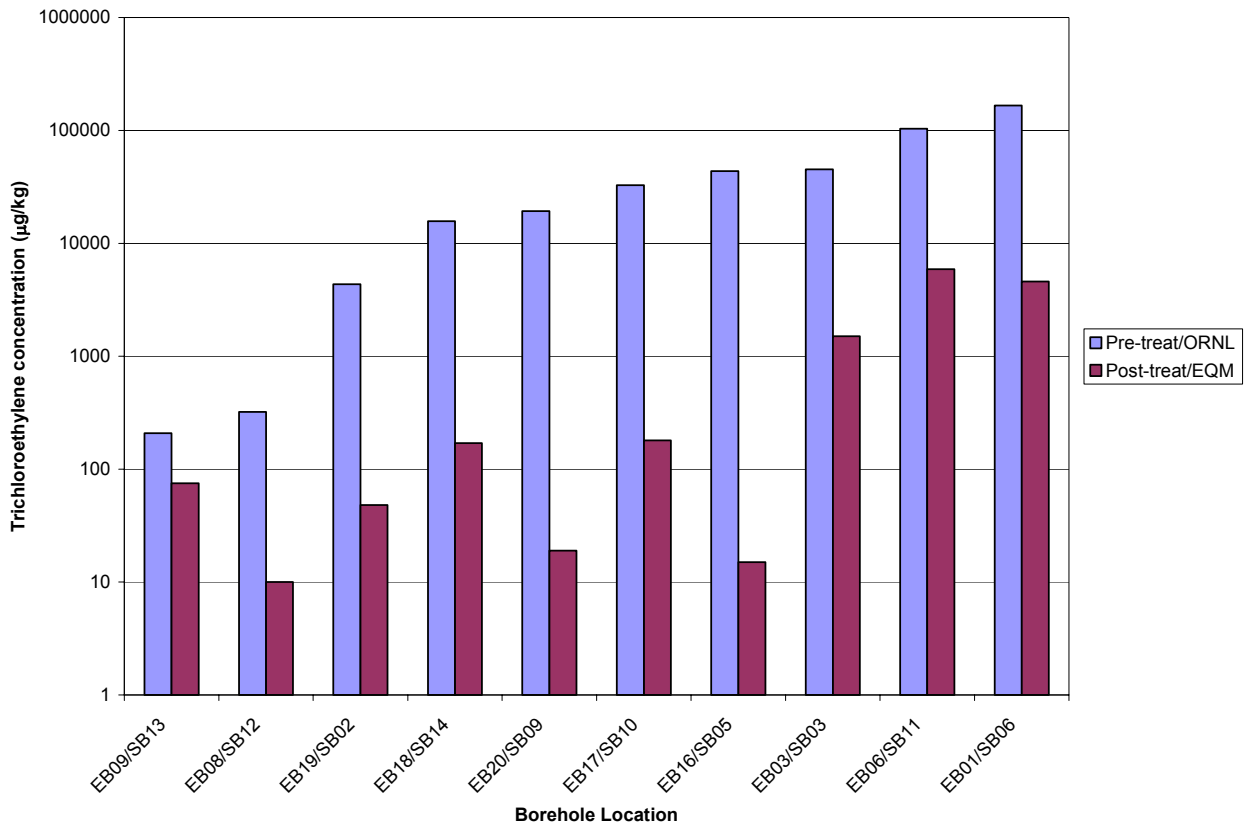


Fig. 3. Comparison of trichloroethylene concentrations in pre- and post-treatment soil samples from 28-ft.

Pre-treatment groundwater samples were obtained by ORNL from temporary 1-in PVC monitoring wells, which were installed in some of the boreholes. Post-treatment samples could not be collected from these temporary wells because well construction data were not available to EQM/CDM. Instead, post-treatment groundwater samples were collected from four permanent Gallia monitoring wells in the vicinity of the

ISCO-LP field test. TCE in Well X701-21G north of the ISCO-LP field test site (see Fig. 2b for location) was measured at 87 ppb, a significant drop from historical TCE concentrations that ranged from 1000 to 10000 ppb. This decrease may be a direct result of the ISCO-LP treatment and/or previous ISCO field demonstrations conducted upstream of this well (West et al. 1998). TCE concentrations in the other three wells sampled after the field test were not significantly different from pretreatment levels.

There were no discernable differences in Mn soil concentrations before and after ISCO-LP. Dissolved Mn in post-treatment groundwater samples ranged from 0.01 to 6.28 mg/L; historical values for the entire X-701B site range from 0.02 to 112 mg/L (EQM/CDM 2001). It appears that the ISCO-LP field test did not lead to significant increases in Mn levels, this may very well be due to the small volume of oxidant that was injected during the field test.

2.5 ACCIDENT DURING NEUTRALIZATION OF EXCESS NaMnO_4 SOLUTION

During the ISCO-LP field test, a field worker was seriously injured from a violent chemical reaction. The field worker was neutralizing approximately 3 gal of sodium permanganate solution of unknown concentration contained in a 5-gal bucket. The solution came mostly from liquids drained or pumped out of the Geoprobe drill rods. Oxidant solution was being delivered to the Geoprobe tip through a pressurized line that was threaded through the drill rods. The reason behind the unexpected buildup of oxidant-laden fluids in the drill rods was not investigated but may be either from leakage of the pressurized line, or from overly rapid or pressurized injection into a saturated low-permeability deposit (i.e., the Minford).

To neutralize the oxidant-laden (purple) liquid, the field worker dropped an unknown amount of crystalline sodium thiosulfate (a strong reducing agent) into the 5-gal bucket. A violent explosion from a steam bubble ensued, which resulted in solution being sprayed at least 15-ft into the air. The field worker was sprayed by the airborne solution and suffered from third degree burns. A drilling assistant, who was standing within a few feet of the explosion, was also sprayed by the airborne solution but was not seriously injured.

For disposal of concentrated (40%) NaMnO_4 solutions, the material safety data sheet (MSDS) for Liquiox (a commercially available concentrated NaMnO_4 solution used for the ISCO-LP field test) recommends dilution to ~6% and reduction with sodium thiosulfate. The health and safety plan for the ISCO-LP field test specified that dilute NaMnO_4 solutions (0 to 6 g/L), including excess injection fluids, will be neutralized with the gradual addition of crystalline sodium thiosulfate. The injection fluid used during the ISCO-LP field test was ~2%, significantly more dilute than what the Liquiox MSDS recommended for neutralization. It is possible that the oxidant-laden liquid drained from the drill rod was not exactly of the same composition and may have been more concentrated than the injection solutions, although it is difficult to see how the latter can occur. The explosion was more likely caused by the rate at which the field worker added the crystalline thiosulfate to the 5-gal bucket of oxidant-laden fluid. Nevertheless, it is apparent that the hazards of the neutralization process were not clearly identified and adequately conveyed to the field workers. A detailed analysis of the accident was conducted by DOE and is documented in an accident investigation report (October 2000, Oak Ridge Operations, US DOE).

3. TECHNOLOGY APPLICABILITY

The following is a list of factors that need to be considered when evaluating the applicability of ISCO-LP for a particular contaminated site.

1. Oxidizability of the target contaminant(s). The chemical oxidant must be capable of degrading the target contaminants under the site-specific geochemical environment. This is best evaluated through laboratory treatability studies using soil/sediment samples from the site.
2. Depth of contamination. Depth limitations are related to the specific drilling equipment that will be used as lances (e.g., the Geoprobe drill rig in the PORTS ISCO-LP field test). Contamination shallower than 100 ft can potentially be treated, but shallower depth constraints may be necessary for certain drill rigs and geotechnical conditions. The depth is also limited by the time required to complete an individual lance penetration, which must be short enough such that areas can be cleaned up within a reasonable amount of time.
3. Areal extent of contamination. ISCO-LP is best applied to hot spots and source zones rather than to large (i.e., mile-long) groundwater plumes.
4. Geotechnical and hydraulic characteristics of contaminated unit. Drilling and oxidant injection rates, and time required for treatment, are affected by the geotechnical and hydrogeological nature of the sediments. ISCO-LP is potentially applicable to low-permeability media but fine-grained and consolidated saturated media may pose problems. The hydrogeologic properties of the Minford at PORTS are probably near the limits of ISCO-LP applicability.
5. Underground man-made structures (i.e., buried pipelines and other utilities, underground storage tanks). These can present short-circuits for the injected fluids. The potential for ISCO-LP to negatively impact such structures both mechanically and chemically should also be evaluated.
6. Vertical accessibility of contamination. Equipment needed for lance permeation must be able to access the contaminated zone from the surface. Drill rigs capable of angled penetrations can be used for contamination under surface structures.
7. Presence of nearby groundwater seeps into surface waters. Permanganate solutions impart a purple color even at very low concentrations. In the long-term, excess permanganate not consumed by contaminants will react with natural organic matter as the oxidant moves through the subsurface. In situations where surface waters are very near the contaminated site, ISCO-LP may cause surface seepage of purple liquid that is aesthetically undesirable.
8. Oxidant demand of contaminated sediments. ISCO probably is not optimal for soils with very high natural organic content because larger amounts of oxidant will be needed, resulting in high treatment costs.
9. Co-contaminant metals. Mobility of some metals (e.g. U, Cr) is strongly influenced by its oxidation state, with mobility increasing at higher oxidation states (e.g U(VI) versus U(IV); Cr(VI) versus Cr(III)). Inadvertent mobilization of co-contaminant metals by ISCO should be considered.

4. COST

The major elements of cost for an ISCO-LP implementation are: (1) reagents (KMnO₄ or NaMnO₄), (2) mobilization, (3) lancing equipment rental/operation, (4) labor costs for field workers (i.e., equipment operators, personnel in charge of mixing oxidant solutions, sampling and performance monitoring, safety officers) and (5) waste disposal. Waste generation generally be limited to excess KMnO₄ or NaMnO₄ solutions, which can be neutralized in the field. (see Section 6 for safety considerations).

The following is a general approach to estimating the cost for ISCO-LP at a given site:

1. Based on site characterization data and laboratory treatability studies, determine the mass of oxidant per unit volume of soil required to degrade the expected mass of contaminants as well as to satisfy the natural oxidant demand.
2. Select the concentration of oxidant solution to be used, based on handling issues (e.g., dilute solutions are more desirable). Using the selected oxidant concentration and required mass of oxidant from (1), calculate the volume of oxidant solution needed per unit volume of soil.
3. Estimate the dispersion radius or radius of influence for an individual lance penetration. This is best achieved through field tests, but as this technology becomes more widespread, general rules-of-thumb will emerge.
4. The dispersion radius is used to determine number of lance penetrations needed to treat a given area.
5. Select the number of injection depth intervals for an individual lance penetration. This is also best achieved through field tests.
6. Calculate the time required to complete an individual lance penetration using the number of injection depth intervals (step 5), the dispersion radius (step 3), amount of oxidant solution needed per volume of soil (step 2), the oxidant injection and the drilling rate (based on operator experience).
7. Calculate the total time required to treat a given area using the estimated number of lance penetrations (step 4) and the time required to complete an individual permeation (step 6).
8. Estimate the number of personnel needed in the field. Calculate the total labor and equipment operation costs for cleaning the entire site based on the total time estimated for treatment (step 7) and unit labor and equipment operating costs.
9. Total treatment cost = labor cost + equipment rental/operating cost + reagent cost + waste disposal + mobilization/travel + plan preparation + permitting + incidental supplies (e.g., mixing equipment, vials for soil samples).

The ITC subcontract for conducting oxidant injections for the ISCO-LP field test at PORTS was priced at \$338K. This subcontract covered process design, preparation of plan, permitting and approval, mobilization, oxidant injections, and report writing. It excluded soil sampling and analysis for

performance monitoring. Thus, based on a 244,800 cu. ft. treatment volume, the unit cost for the ISCO-LP would have been ~\$37/cu.yd. This is a hypothetical cost because the field test was not completed as planned.

5. REGULATORY, SAFETY, AND HEALTH CONSIDERATIONS

5.1 REGULATORY AND PLANNING DOCUMENTS

A number of regulatory considerations were addressed before deployment of the ISCO-LP field test. The permits and paperwork that was prepared is listed below:

- Health and Safety Plan,
- Underground Injection Permit
- Comprehensive Environmental Recovery, Compensation, and Liability Act (CERCLA)
- Resource Conservation and Recovery Act (RCRA)
- National Environmental Protection Act review was required

In case of field tests, additional requirements are,

- Environmental Technology Section Procedures which included a Technical Work Plan,
- Generator's Waste Management Plan,
- Quality Assurance Project Plan,
- Prior to deployment of the lance permeation portion of the contract, a Site Operational Review Committee document was submitted. This evaluated project readiness to start work which includes:
 1. summary description of scope of the work,
 2. review needs evaluation form,
 3. project schedule,
 4. project location,
 5. list of plans and relevant work,
 6. process controls,
 7. training requirements,
 8. activity hazard analysis

5.2 SAFETY, RISKS, BENEFITS, AND COMMUNITY REACTION WORKER SAFETY

- Worker safety risks are those associated with work at a contaminated site especially handling of hazardous chemicals and association with standard construction operations.
- Major potential risk to workers can occur during the handling of the reactive oxidant (e.g., concentrated permanganate solution). The NaMnO_4 solution is a strong oxidizer and has to be kept away from combustibles. Spills have to be avoided and this material must be isolated from sparking equipment.
- A vital lesson learned from the ISCO-LP field test is that a clear understanding of the hazards of the neutralizing process (using thiosulfate for reducing excess permanganate solutions) must

be conveyed to field workers. Precise instructions on how to handle and neutralize oxidant solutions must be provided.

- A prerequisite for all field personnel is a 40-h Occupational Safety and Health Administration training. This is a requirement in the 29 Code of Federal Regulations (CFR) 1910.120 for hazardous waste operations.

5.3 COMMUNITY SAFETY

- The chemicals used for ISCO-LP pose no hazard to the community as a whole due to their low concentrations after dispersal into the soil and groundwater.
- The by-products generated are also not considered to be harmful to the community. These are CO₂, MnO₂ solids, cations (e.g., sodium and potassium), and halides.
- In situ chemical oxidation using KMnO₄ and NaMNO₄ does not cause release of volatile organic compounds.
- Transportation safety concerns are covered by the subcontracting agencies. There have been no unusual or significant concerns in connections with materials and equipment used in this technology.

5.4 ENVIRONMENTAL IMPACTS

Summarizing the points addressed in “Community Safety” the environmental impacts are as follows:

- Potassium permanganate and sodium permanganate are considered to be safe in the environment since the concentration is very low when it is dispersed into the soil and groundwater.
- Negligible by-products have been mentioned in the preceding paragraph.
- No volatile organic compounds are produced due to oxidation of the contaminants.

5.5 SOCIOECONOMIC IMPACTS AND COMMUNITY PERCEPTION

It is well known that the economic and labor force impacts are minimal in case of implementing in situ remediation technologies used for DNAPLs.

The familiarity of the general public with in situ technologies such as chemical oxidation using potassium and sodium permanganate is low, but explaining and education of the public can be accomplished with ease since these technologies are similar to wastewater treatment methods.

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Purchase order and Statement of Work from UT-Battelle Subcontract number 4000001075, February 14, 2000. Vendor: International Technology Corp, 312 Directors Drive, Knoxville, TN 37923-4799.

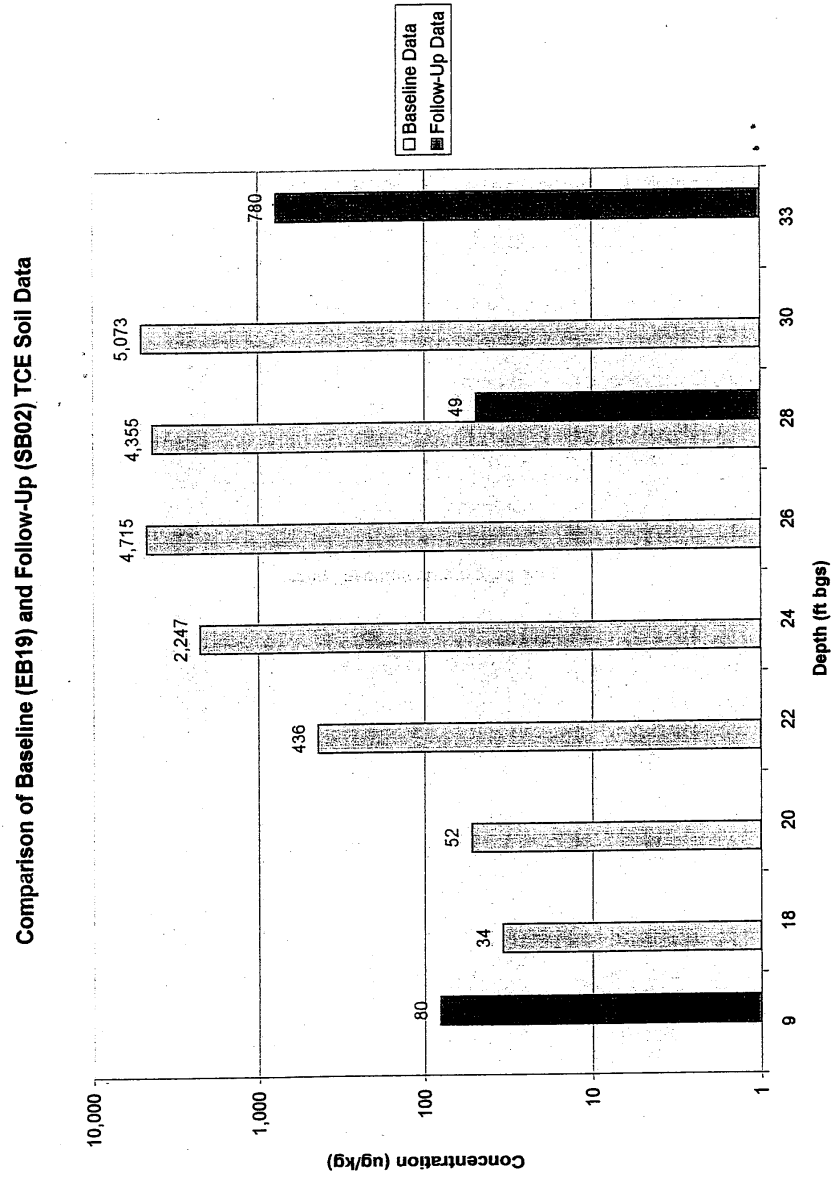
EQ Midwest, Inc./CDM Federal Programs Corporation. October 2001. Evaluation of the X-701B In situ Chemical Oxidation Injection Site at the Portsmouth Gaseous Diffusion Plant, Piketon, OH. DOE/OR/11-3090&D1.

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APPENDIX

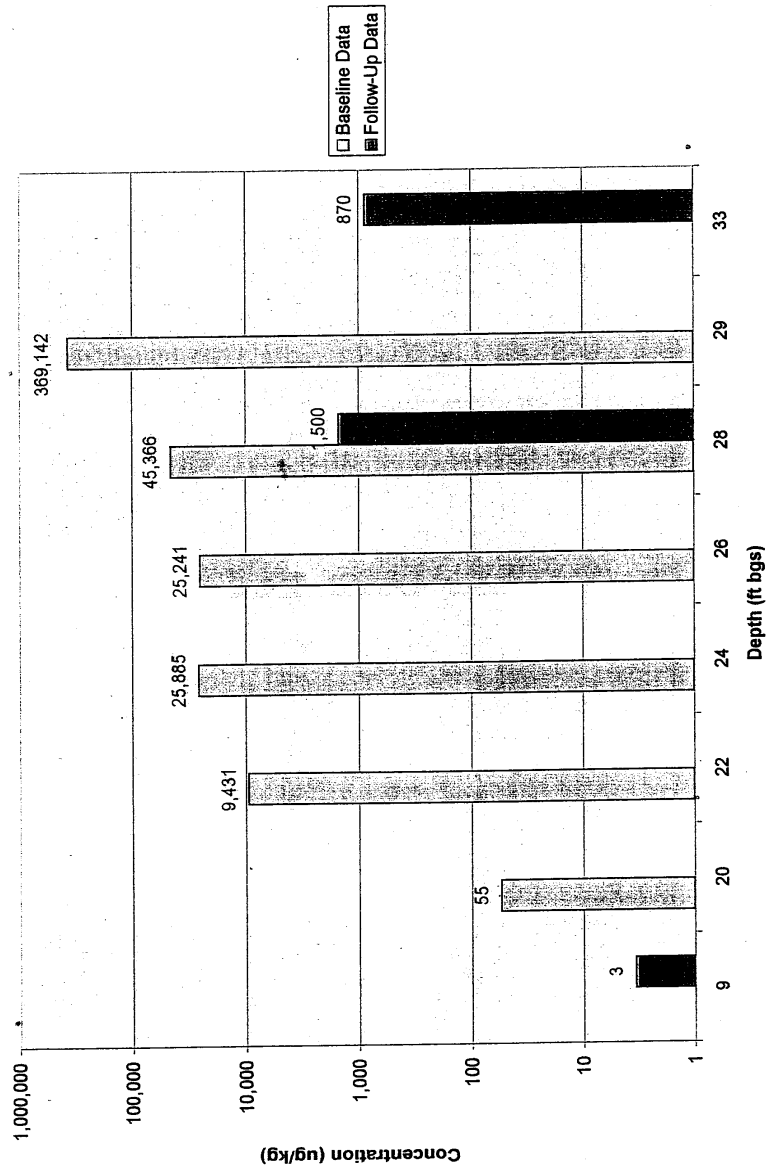
APPENDIX A:

COMPARISON OF PRE- AND POST-ISCO-LP TREATMENT
TCE CONCENTRATIONS (EQM/CDM 2001)

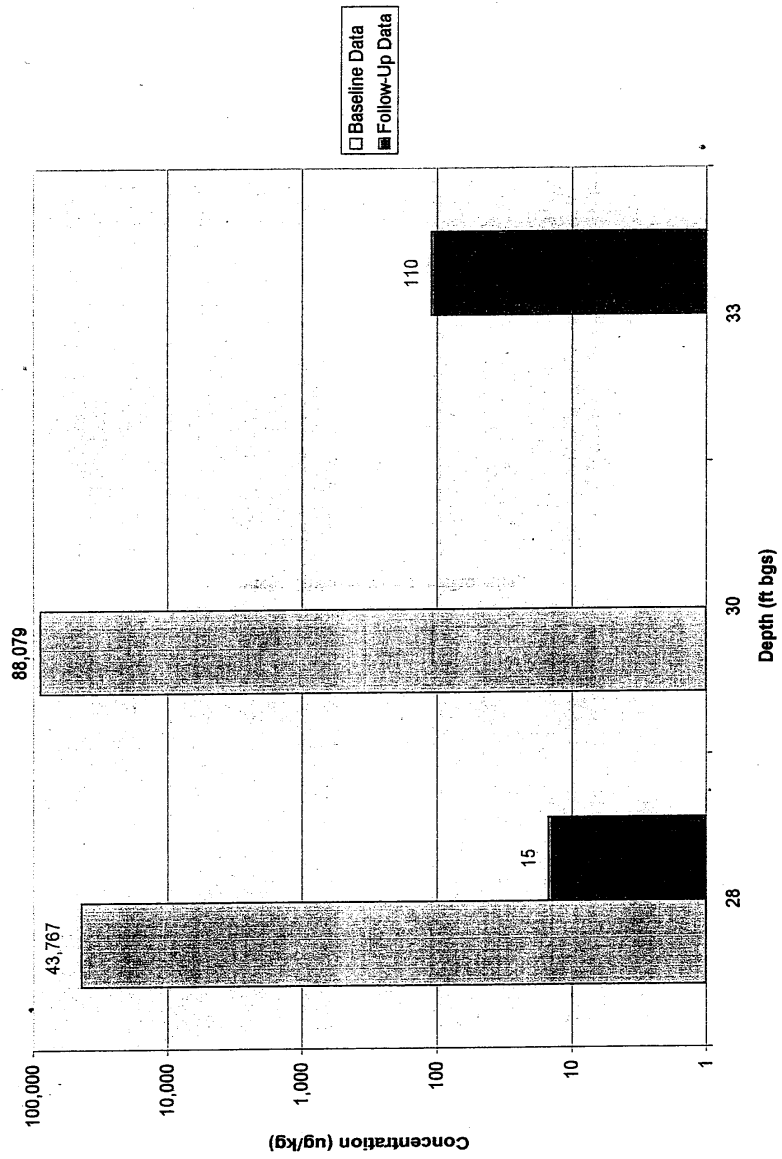


D-3

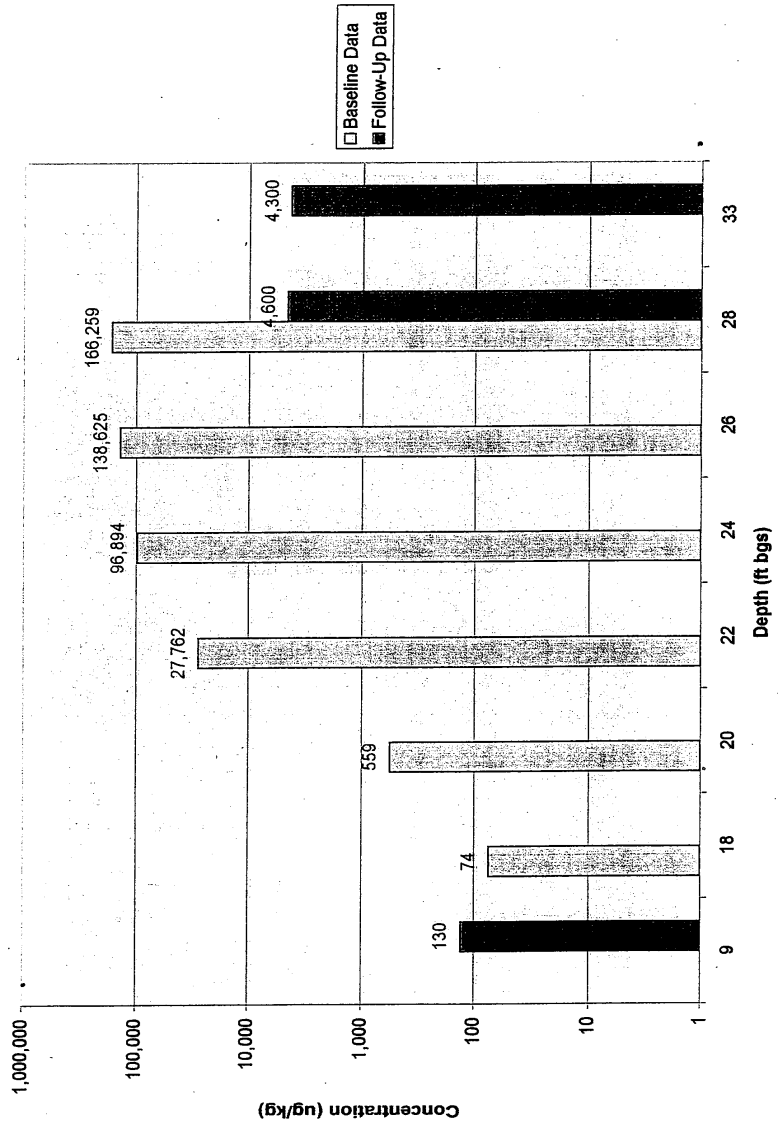
Comparison of Baseline (EB03) and Follow-Up (SB03) TCE Soil Data



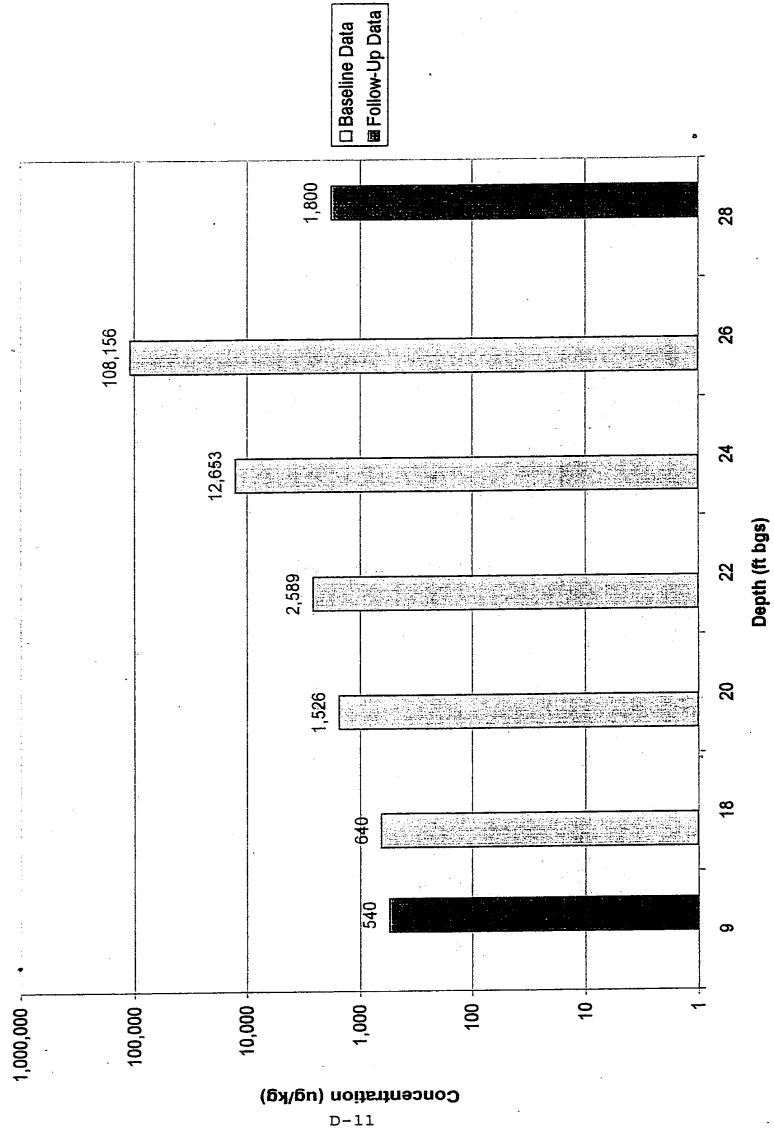
Comparison of Baseline (EB16) and Follow-Up (SB05) TCE Soil Data



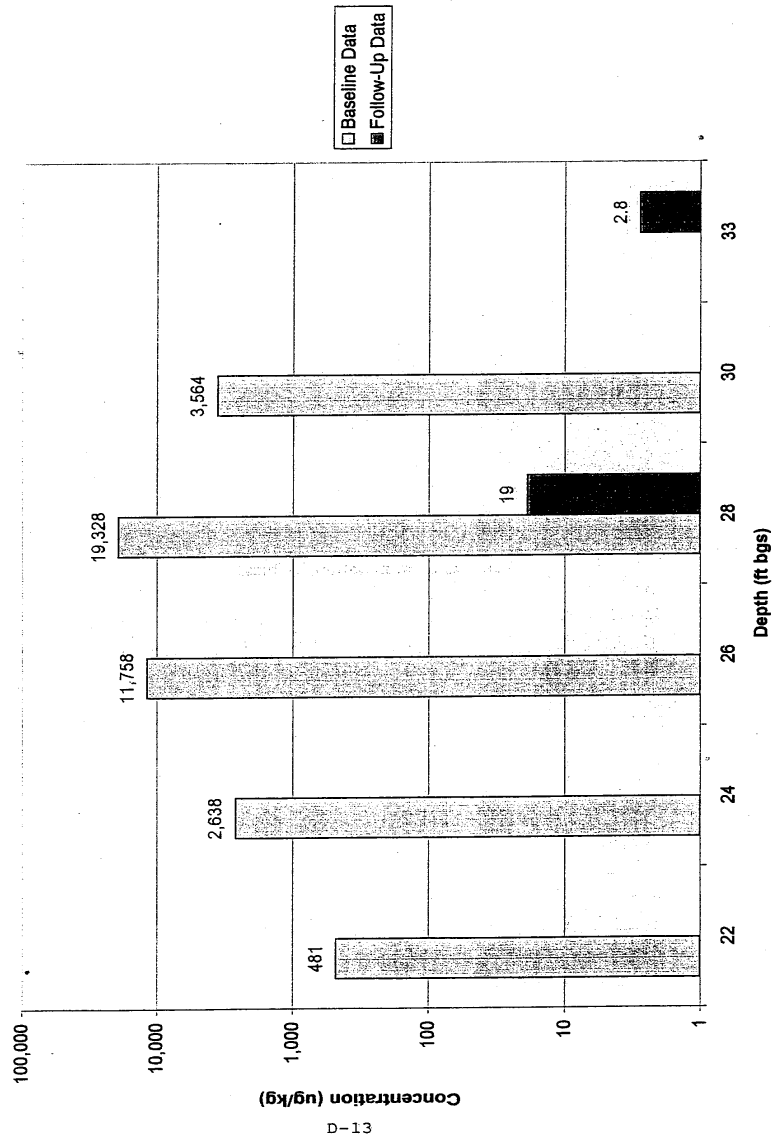
Comparison of Baseline (EB01) and Follow-Up (SB-06) TCE Soil Data



Comparison of Baseline (EB05) and Follow-Up (SB07) TCE Soil Data

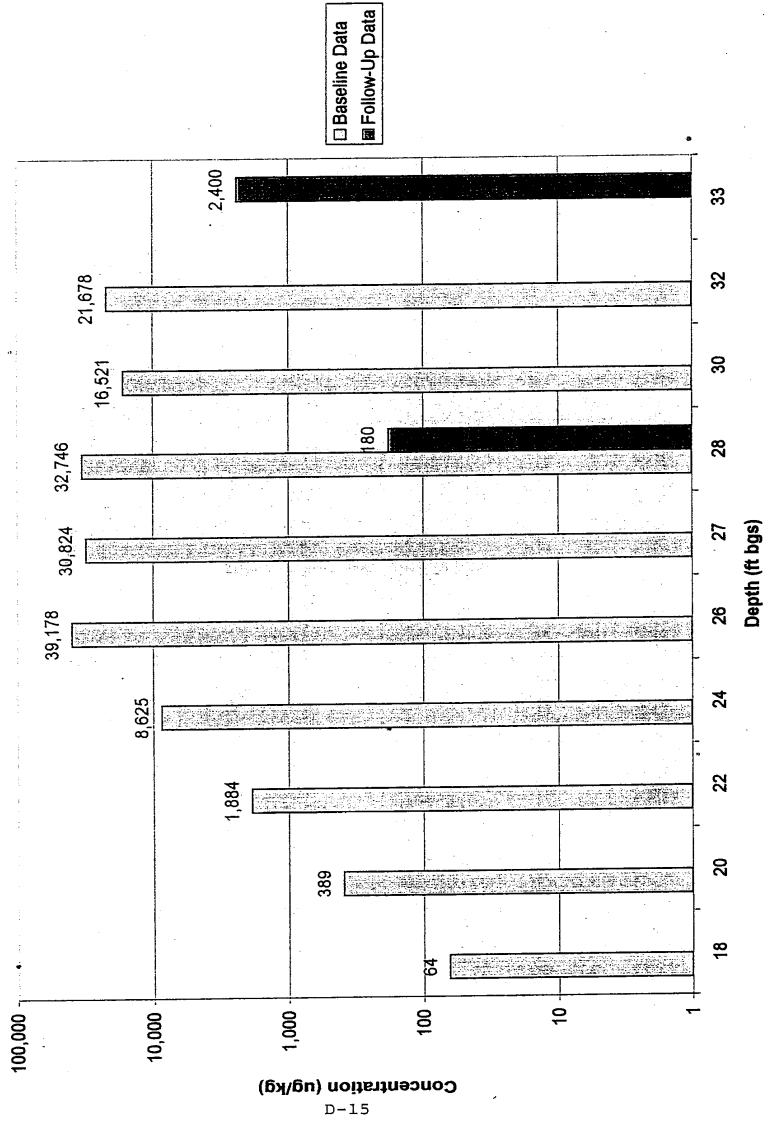


Comparison of Baseline (EB20) versus Follow-up (SB09) TCE Soil Data

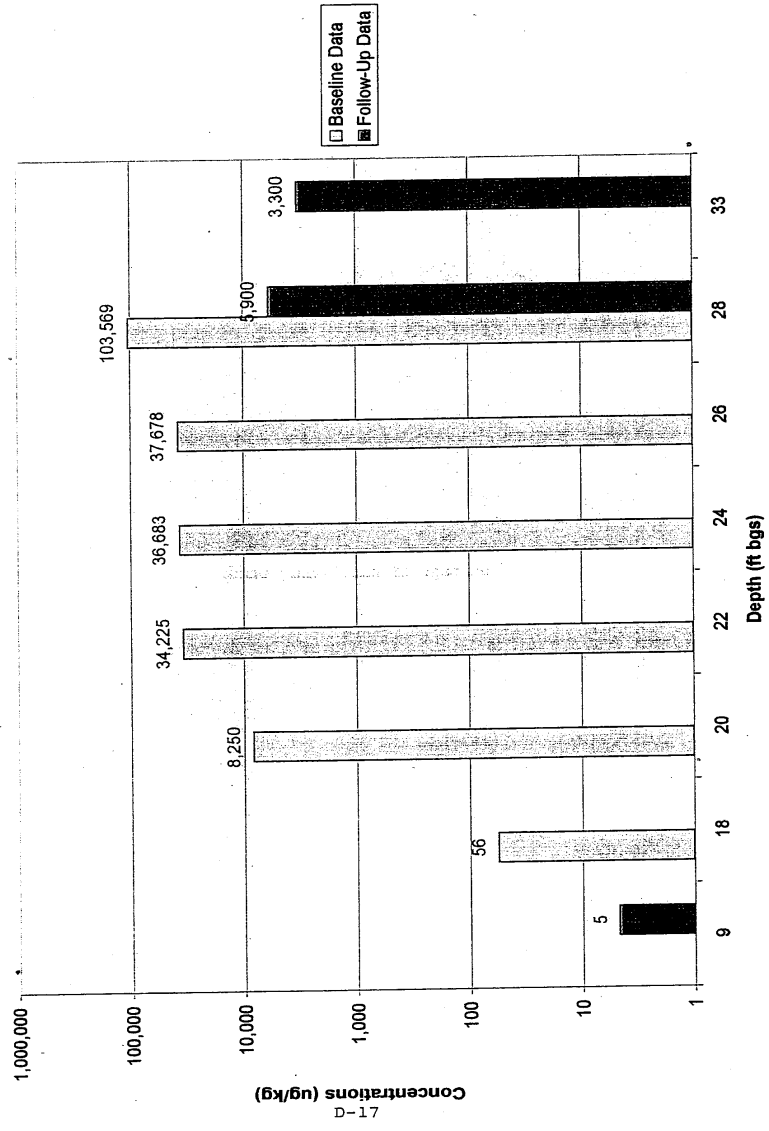


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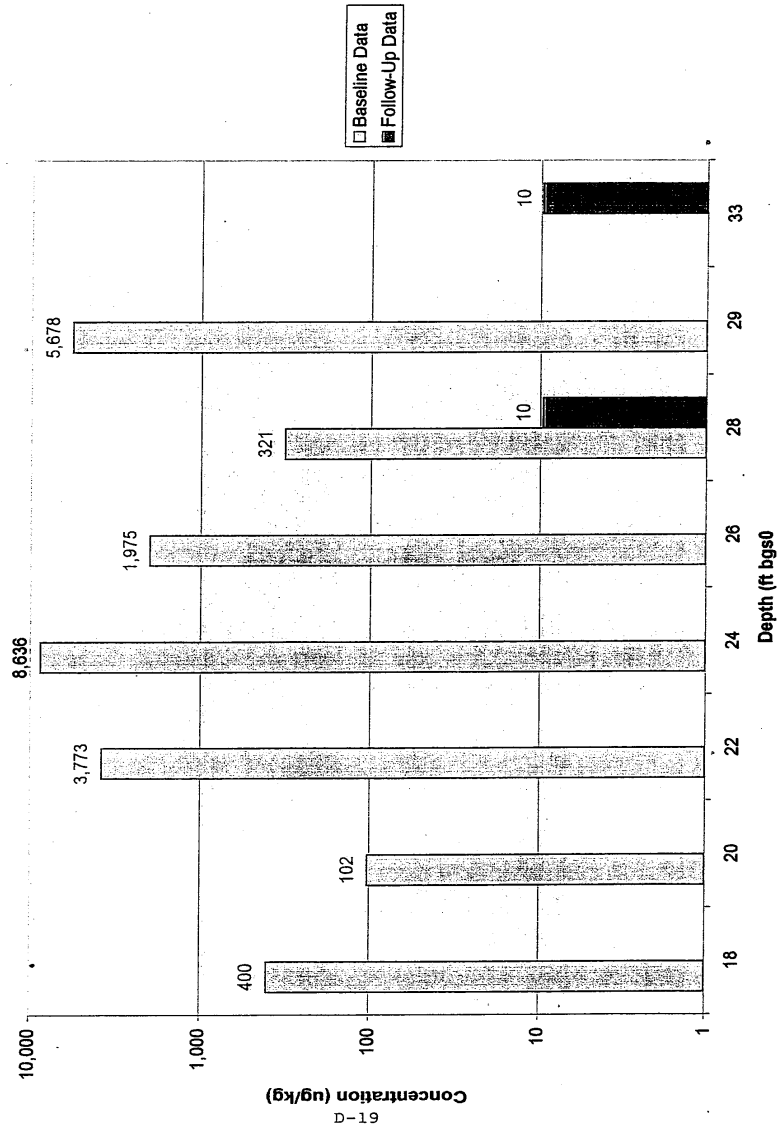
Comparison of Baseline (EB17) and Follow-Up (SB10) TCE Soil Data



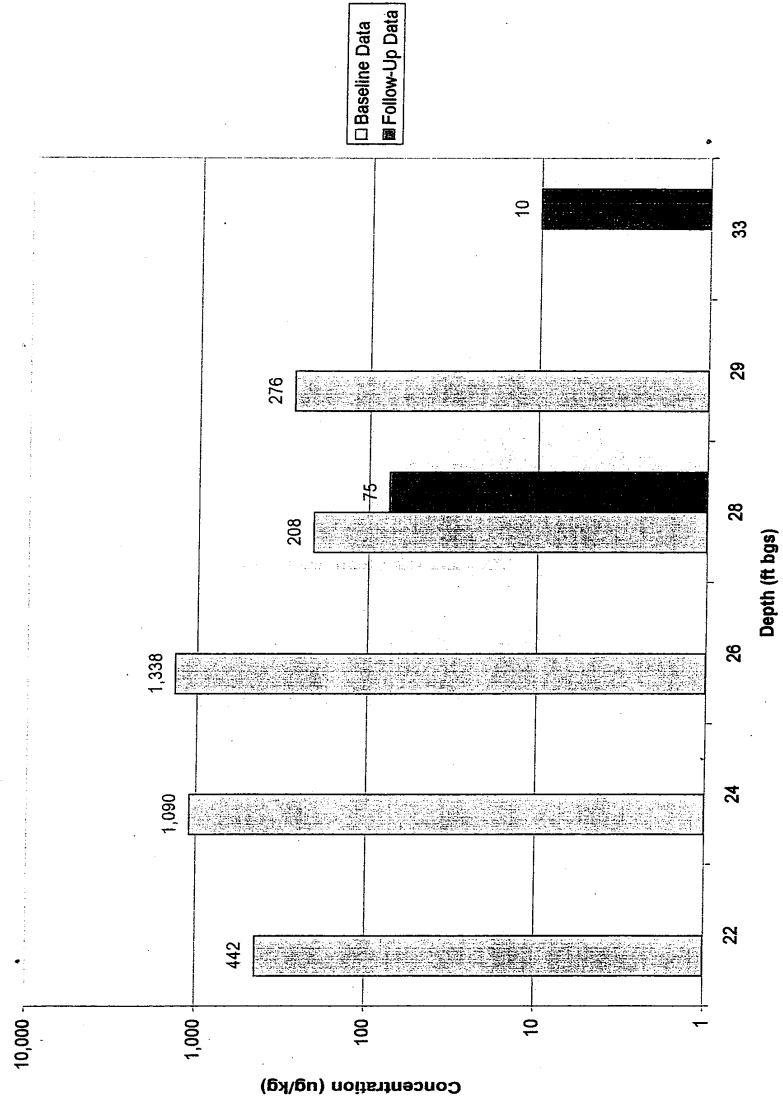
Comparison of Baseline (EB06) and Follow-up (SB11) TCE Soil Data



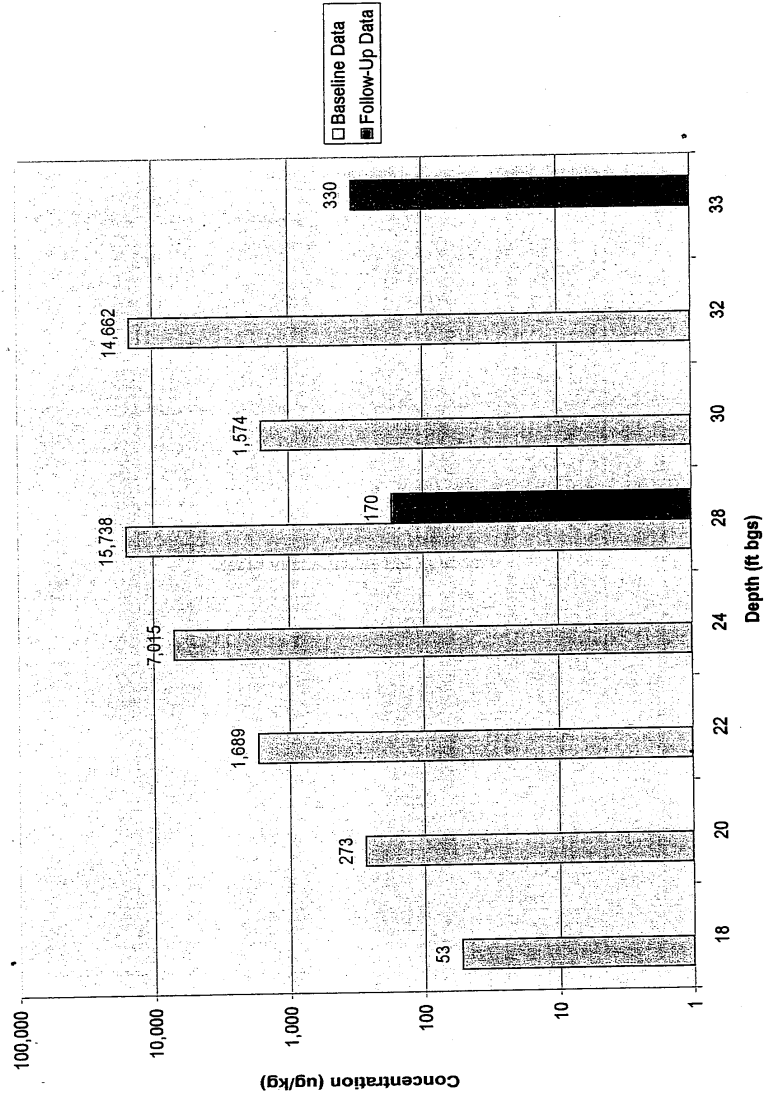
Comparison of Baseline (EB08) and Follow-Up (SB12) TCE Soil Data



Comparison of Baseline (EB09) and Follow-Up (SB13) TCE Soil Data



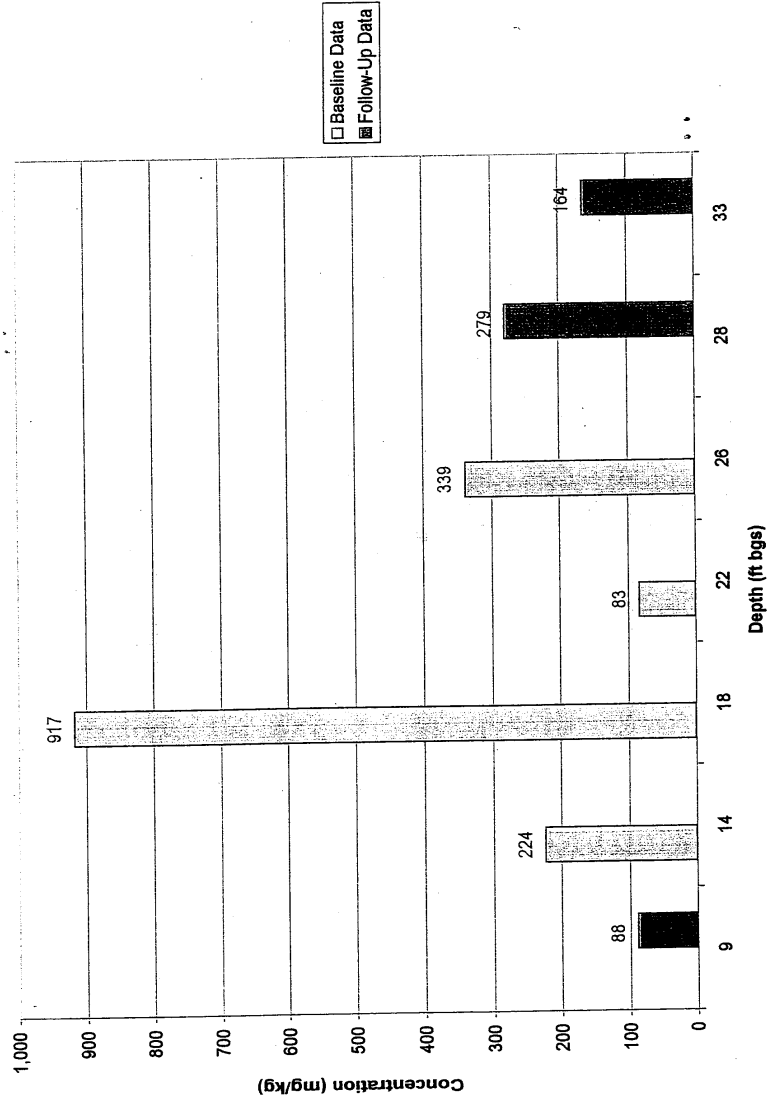
Comparison of Baseline (EB18) and Follow-Up (SB14) TCE Soil Data



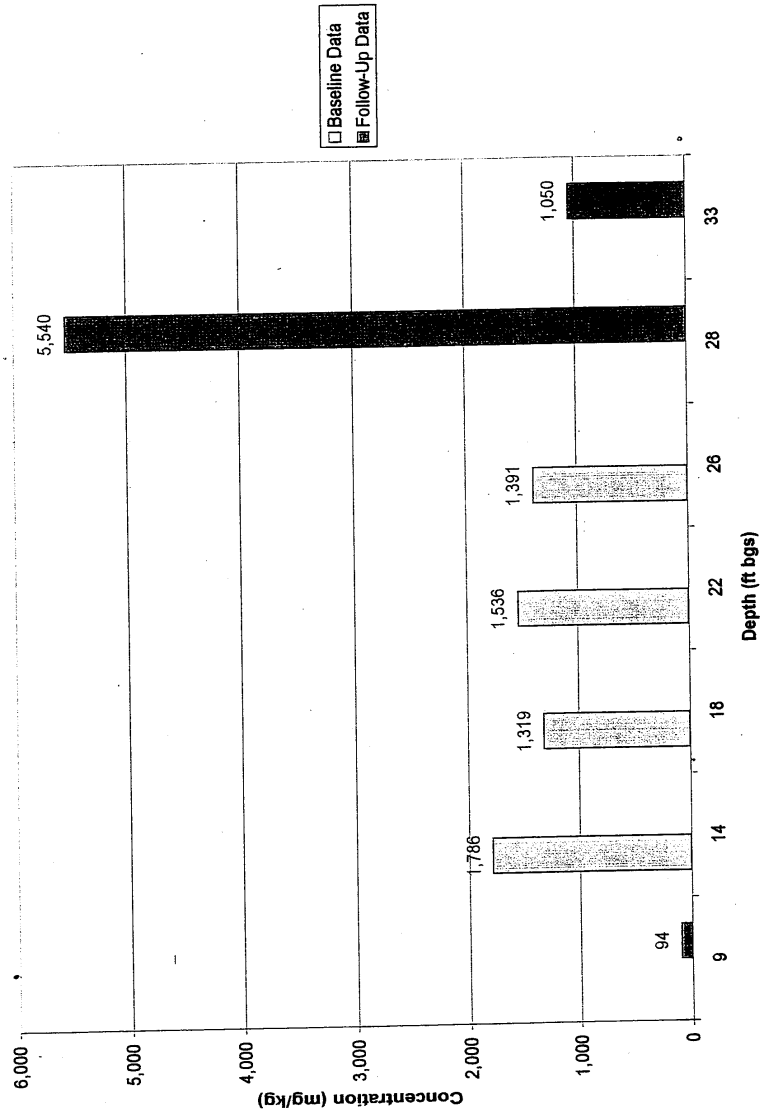
APPENDIX B:

COMPARISON OF PRE- AND POST-ISCO-LP TREATMENT
MANGANESE SOIL CONCENTRATIONS

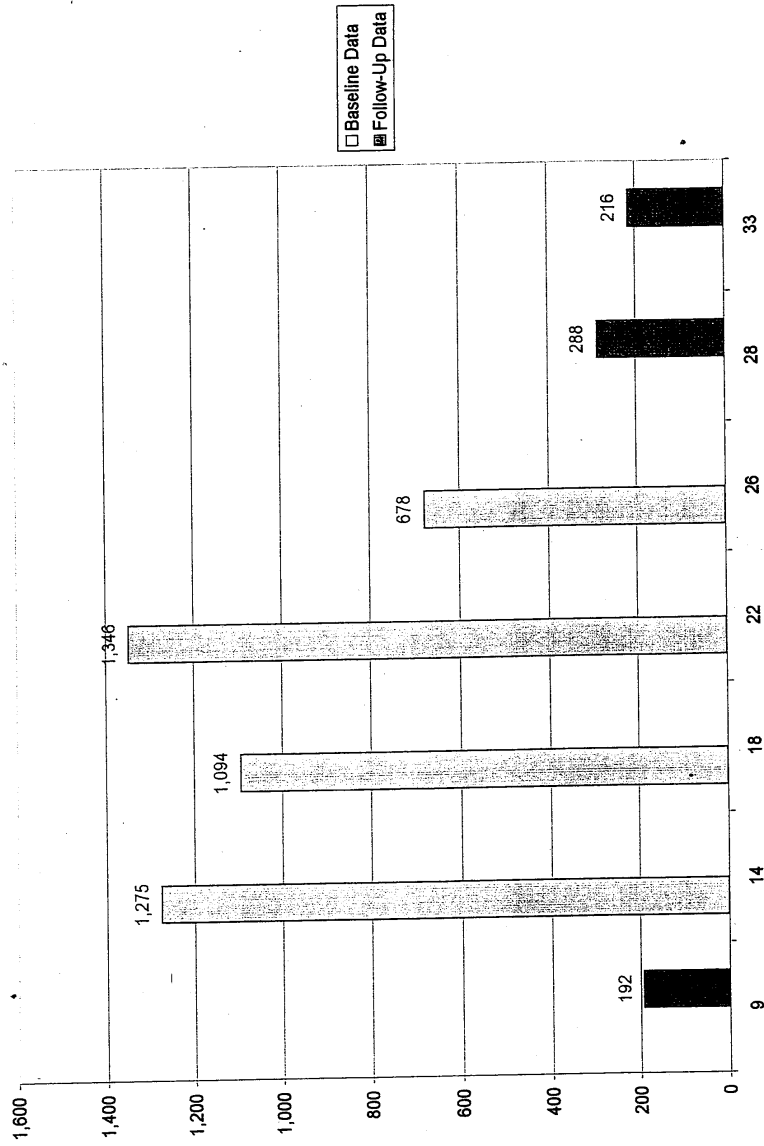
Comparison of Baseline (EB04) and Follow-Up (SB03) Manganese Soil Data



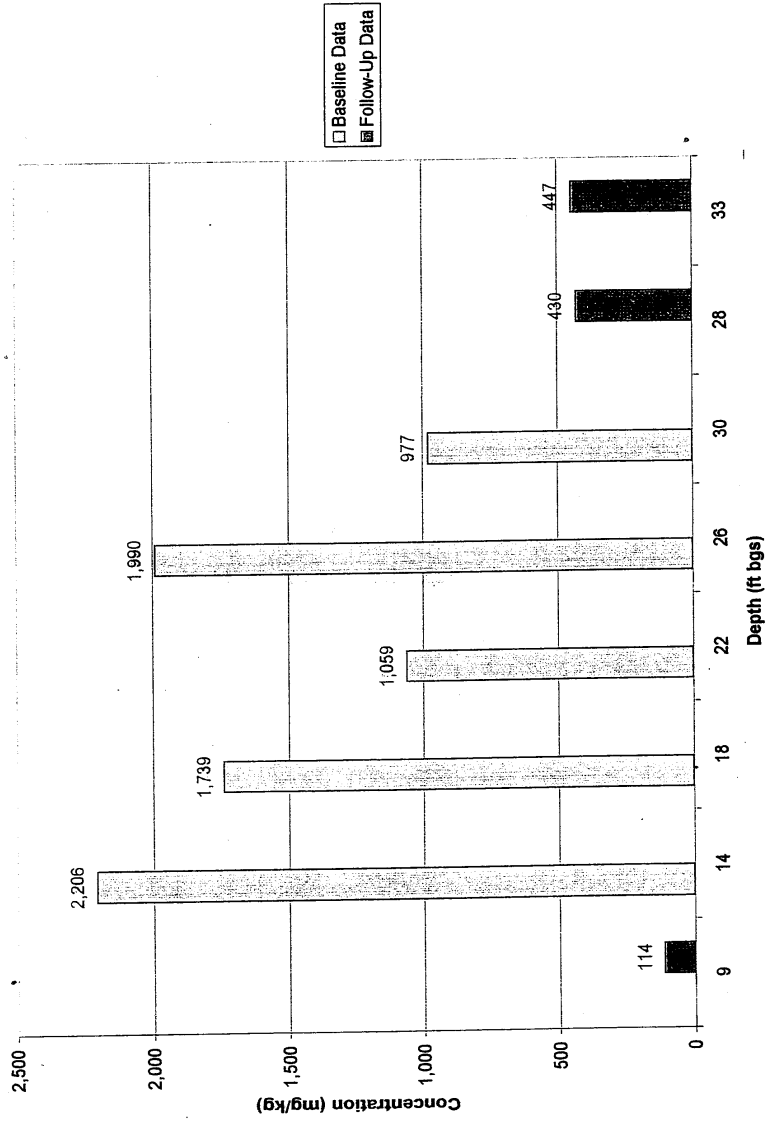
Comparison of Baseline (EB16) and Follow-Up (SB05) Manganese Soil Data



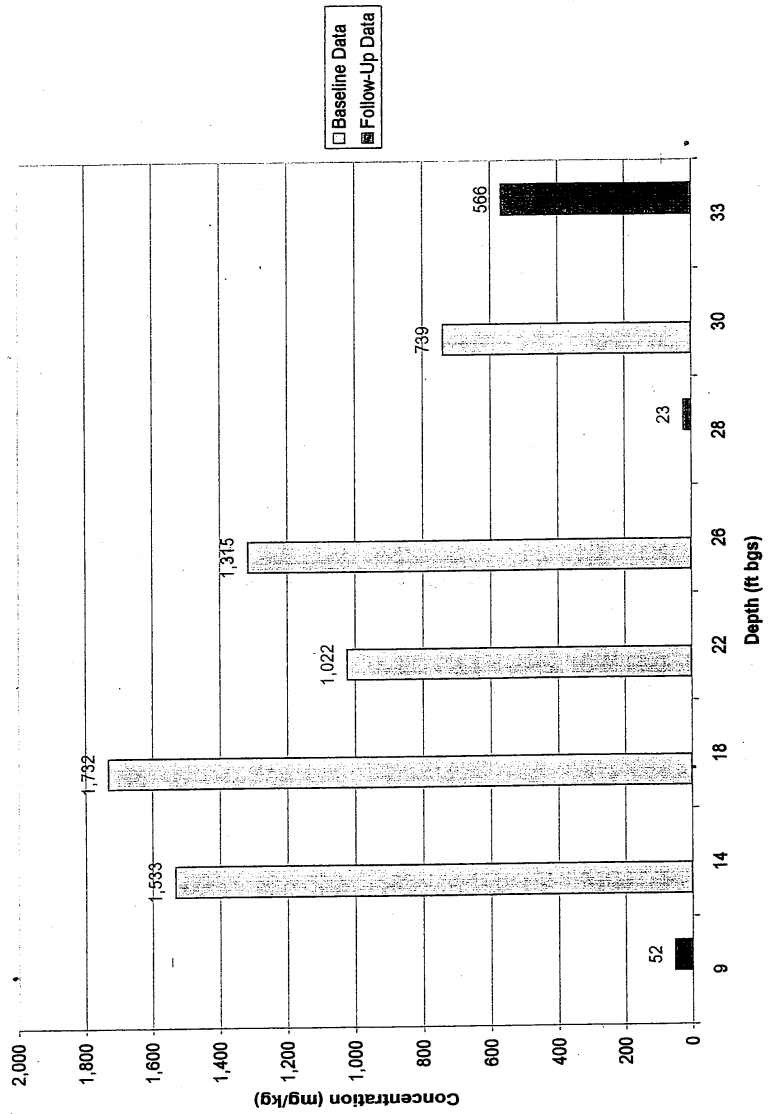
Comparison of Baseline (EB05) and Follow-Up (SB07) Manganese Soil Data



Comparison of Baseline (EB12) and Follow-Up (SB08) Manganese Soil Data



Comparison of Baseline (EB18) and Follow-Up (SB14) Manganese Soil Data



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